## Comparative Adsorption Isotherm Study of the Removal of Pb2+ and Zn2+ Onto **Agricultural Waste**

### Olalekan A.P., Dada A. O., Okewale A.O.

Abstract— The removal of lead (II) ions (Pb2+) and Zinc (II) ions from aqueous solution by phosphoric acid modified rice husk has been investigated. Isotherms studies were carried out by considering the equilibrium sorption of Pb2+ and Zn2+. The adsorption isotherms of Pb2+ and Zn2+ ions fitted the Langmuir, Freundlich, Temkin and Dubinin-Radushkevich models well. The highest coefficient of determination values (R2) for Pb2+ was obtained from the Temkin model as 0.997 while that of Zn2+ was obtained from the Langmuir model as 0.990 respectively. The maximum adsorption capacity predicted by the Langmuir Isotherm for Pb2+ and Zn2+ are 142.857 mg/g and 100 mg/g respectively. Isotherm parameters estimated from Langmuir, Freundlich Temkin and Dubinin-Radushkevich showed better adsorption of Pb2+ than Zn2+ under the same experimental conditions. The study showed that rice husk modified with phosphoric acid is an effective low-cost adsorbent for the removal of Pb2+ and Zn2+ from wastewater.

Index Terms— Adsorption, Heavy metals, Rice husk, Langmuir isotherms, Freundlich isotherm, Temkin isotherm, Freundlich isotherm, Dubinin-Radushkevich isotherm .

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#### INTRODUCTION 1

Increase in industrial and mining activities has led to various deterioration of the ecosystem and therefore posed dangers to human health and environment [1]. Heavy metals are some of the toxic pollutants released into water bodies due to various anthropogenic activities. There are many physical and chemical processes for removing metal ions from solution. Examples of such processes include chemical precipitation, ultrafiltration, solvent extraction, and membrane separation [2]. The major disadvantage of these processes is their high operational cost. However, Adsorption, a surface phenomenon, has shown great promise in removing metal ions from solution of wastewater. Commercial activated carbon has been proven as an efficient adsorbents but its cost is prohibitive [3]. Several biosorbents such as rice husk, spent grain, peat, sawdust, and green algae have been researched for the adsorption of metal ions in aqueous solutions [2], [3], [4], [5], [6]. They combine the advantages of being readily available in large quantities, cheap and are environmentally friendly [7].

In this study, rice-husk modified with phosphoric acid was tested for its ability to remove Pb2+ and Zn2+ from synthetic

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wastewater. Rice husk is the hard covering of rice grains obtained from the threshing of rice. An estimated world production of rice husk in 2010 was given as 154 million tons [8].

The objective of this study is to investigate the adsorption of Zn<sup>2+</sup> and Pb<sup>2+</sup> by modified rice husk from aqueous solution. Isotherms of their sorption were studied and compared.

#### 2.0 Materials and Methods

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#### 2.1. Sorbents and sorbates

Rice husk collected at a mill in Ilorin, Kwara, Nigeria, was screened and washed with deionized water to remove impurities and thereafter dried in the oven at 105°C for 2 hours. It was then ground and sieved in a sieve between the range of 150 µm and 250µm. The sieved rice husk was then treated with 1.0M phosphoric acid (H<sub>3</sub>PO<sub>4</sub>) and then heated on the magnetic stirrer at 100°C till it formed a paste. The rice husk paste was the washed in deionized water until the pH is about 6. It was then dried in the oven at  $80^{\circ}$ C. The modified rice husk was tagged phosphoric acid modified rice husk (PRH).

#### 2.2. Preparation of aqueous solution

Stock solutions containing 1000mg/l each of Pb<sup>2+</sup> and Zn<sup>2+</sup> were prepare with distilled water using Pb(NO<sub>3</sub>)<sub>2</sub> and Zn(NO<sub>3</sub>)<sub>2</sub> respectively. Working concentrations in the range of 10 - 200 mg/l were prepared through serial dilution.

#### 2.3. Adsorption Experiments

The experiments were carried out in the batch mode. 0.1 g of the adsorbent, PHR was added to a 100cm<sup>3</sup> of the different concentra-**IJSER © 2014** 

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tions of the synthetic wastewater samples in a 250 cm<sup>3</sup> Pyrex conical flask. The conical flasks were shaken in a orbital shaker at room temperature for 90minutes at 200rpm. The mixtures were filtered with whatman filter paper No 42, and the residual concentration of the filtrate was analyzed using Atomic Absorption Spectrophotometer (2380 UNICAM AAS). The amount of metal ion adsorbed (mg/g) was calculated using the formulae reported by Vanderborght and Van Grieken [9]:

$$q_e = \frac{v(C_i - C_e)}{w} \tag{1}$$

where  $\mathbf{q}_{e}$  is the amount of metal ion sorbed (mg/g);  $C_{e}$  is equilibrium concentration (mg/dm<sup>3</sup>);  $C_{i}$  is initial concentration(mg/dm<sup>3</sup>); w is the weight in gram of the adsorbent.

#### 3. RESULTS AND DISCUSSION

The sorption isotherms of  $Zn^{2+}$  and  $Pb^{2+}$  were studied by fitting the obtained data to Langmuir, Freundlich, Temkin and Dubinin-Radushkevich Isotherm models.

#### 3.1. Langmuir isotherms

The Langmuir isotherm [10] has been widely applied in adsorption studies. It assumes a monolayer adsorption in which adsorbates are adsorbed to a finite number of definite localized sites that are identical and equivalent with no lateral interaction [1].

$$q_e = \frac{q_m K_L C_e}{1 + K_L C_e} \tag{2}$$

Where  $C_{e}$  is the equilibrium concentration (mg/dm<sup>3</sup>);  $q_{e}$  is the amount of metal ions adsorbed (mg/g);  $q_{m}$  is the maximum monolayer coverage (mg/g); *K* is the Langmuir constant (dm<sup>3</sup>/mg).

Foo and Hameed [1] gave the linear forms of the equation as follows:

$$\frac{C_e}{q_e} = \frac{1}{K_L q_m} + \frac{C_e}{q_m} \tag{3}$$

$$\frac{1}{q_e} = \frac{1}{q_m} + \frac{1}{K_L q_m C_e} \tag{4}$$

$$q_{e} = q_{m} - \frac{q_{e}}{K_{L}C_{e}}$$
(5)

$$\frac{q_e}{C_e} = K_L q_m - K_L q_e \tag{6}$$

Parameters such as  $q_{mv}$  and  $K_L$  are obtained by making the appropriate plots using any of the equations (3) – (6).

For Pb<sup>2+</sup>, applying the linear form of Langmuir equation, Equation (3), with the plot of  $C_{e}/q_{e}$  against  $C_{e}$  gave a value of R<sup>2</sup>. For Zn<sup>2+</sup>,

Equation (4) gave the best  $\mathbb{R}^2$  with the plot of  $\frac{1}{q_e}$  against  $\frac{1}{C_e}$ . With these, isotherms parameters which are useful for adsorption system design were obtained and reported in Table 1.

Webber and Chakkravorti [11] defined a dimensionless constant  $R_L$  known as Separation factor as:

$$R_L = \frac{1}{1 + K_L C_0} \tag{7}$$

Where  $K_L$  (L/mg) is the Langmuir constant and  $C_0$  is the adsorbate initial concentration. The value of  $R_L$  indicates the nature of adsorption as either unfavourable ( $R_L$ >1), linear ( $R_L$ =1), favourable ( $0 < R_L < 1$ ) or irreversible ( $R_L = 0$ ). From the estimated values of  $R_L$ in Table 1, it can be concluded that  $Zn^{2+}$  and  $Pb^{2+}$  adsorption on modified rice husk is favourable. However, the i smaller value for  $Pb^{2+}$  compared to that of  $Zn^{2+}$  indicates that the sorption of  $Pb^{2+}$  is more favourable.

#### 3.2. Freundlich isotherm

Freundlich isotherm was developed to study the adsorption of a material onto animal charcoal [12]. It is, however, presently applied in heterogeneous systems especially for organic compounds or highly interactive species on activated carbon and molecular sieves. It is n empirical model which applies to multilayer adsorption, with nonuniform distribution of adsorption heat and affinities over the heterogeneous surface [1].

The equation is expressed as:

$$q_{e} = K_{F} C_{e}^{1/n} \tag{8}$$

The equation can be expressed in its linear form as:

$$\ln q_s = \ln K_F + \frac{1}{n} \ln C_s \tag{9}$$

 $K_F$  is the Freundlich constant related to the adsorption capacity, where 1/n is related to the adsorption intensity. A plot of  $\ln q_e$ against  $\ln C_e$  gives 1/n and  $\ln K_F$  as the slope and the intercept respectively. 1/n value below one implies chemisorptions while a value above one indicates cooperative adsorption [1]. Also, 1/n is a heterogeneity parameter. The smaller the value, the greater the heterogeneity of the adsorption process. If the value *n* lies between one and ten, then adsorption is said to be favourable [13]. The values of 1/n for  $\text{Zn}^{2+}$  adsorption is 0.631 while that of Pb<sup>2+</sup> is 0.178. This shows that the adsorption of Pb<sup>2+</sup> is more unto heterogeneous surface than that of Zn<sup>2+</sup>. Sorption of Zn<sup>2+</sup> and Pb<sup>2+</sup> onto modified rice husk is favourable as the values of *n* in both cases lie between 1 and 10. International Journal of Scientific & Engineering Research, Volume 5, Issue 4, April-2014 ISSN 2229-5518

modified rice husk is favourable as the values of n in both cases lie between one and ten.

### 3.3. Temkin isotherm

Temkin isotherm contains a factor that takes into account the adsorbent-adsorbate interactions [14]. The model is given as:

$$q_{e} = \frac{RT}{b_{T}} \ln A_{T} C_{e} \tag{10}$$

The linear form is expressed as:

$$q_{s} = \left(\frac{RT}{b_{T}}\right) lnA_{T} + \left(\frac{RT}{b_{T}}\right)$$

where

 $A_T$  = Temkin isotherm equilibrium binding constant (L/g),

 $b_T$  = Temkin isotherm constant,

R = universal gas constant (8.314 J/mol.K),

T = Temperature at 298 K.

The equilibrium adsorption of  $Pb^{2+}$  is better represented by Temkin isotherm than for  $Zn^{2+}$ . However, Temkin isotherm gives a good fit for both  $Pb^{2+}$  and  $Zn^{2+}$  with high  $R^2$  values. In fact, the isotherm gave the best fit for  $Pb^{2+}$  out of the all the isotherms fitted to the adsorption data with an  $R^2$  value of 0.997.

#### 3.4. Dubinin-Radushkevich isotherm

Dubinin-Radushkevich isotherm [15] is an empirical model generally applied to express the adsorption of subcritical vapours onto micropore solids following a pore filling mechanism [16]. It is expressed as:

$$q_s = (q_s)exp(-k_{ad})\varepsilon^2 \tag{12}$$

where

 $q_e$  = amount of adsorbate in the adsorbent at equilibrium(mg/g);

 $q_s$  = theoretical isotherm saturation capacity (mg/g);

 $K_{ad}$  = Dubinin–Radushkevich isotherm constant (mol<sup>2</sup>/kJ<sup>2</sup>)

E can be correlated as:

$$\varepsilon = RT \ln \left[ 1 + \frac{1}{C_s} \right] \tag{13}$$

where *R*, *T* and  $C_{g}$  are the gas constant (8.314 J/mol.K), absolute temperature (K) and adsorbate equilibrium concentration (mg/L) respectively.

The linear form of the Dubinin–Radushkevich isotherm is obtained by taking the logarithm of the equation.

$$ln(q_s) = ln(q_s) - k_{ad}\varepsilon^2$$
(14)

The model has often successfully fitted high solute activities and the intermediate range of concentrations data well.

 $K_{ad}$  is related to the free energy of sorption / mole of the sorbate as it migrates to the surface of the adsorbent from infinite from infinite distance in the solution [18]. The apparent energy of adsorption from Dubinin–Radushkevich model can be computed using the relationship [20]:

$$E = \frac{1}{\sqrt{2k_{ad}}} \tag{15}$$

**(11)** The apparent energy of adsorption of  $Pb^{2+}$  is much lower than that of  $Zn^{2+}$ . This explains why higher adsorption of was observed.

The model gave a better fitting for  $Pb^{2+}$  with a high  $R^2$  of 0.944 while a  $R^2$  of 0.793 was obtained for  $Zn^{2+}$ . Dubinin–Radushkevich isotherm constant was obtained and reported in Table 1.

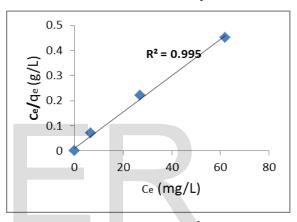


Fig. 1. Langmuir isotherm plot for Pb<sup>2+</sup>

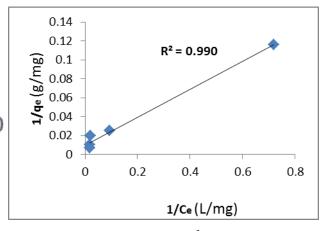


Fig 2. Langmuir isotherm plot for Zn<sup>2+</sup>

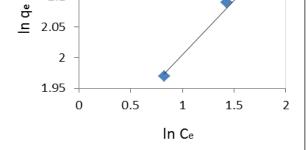


Fig. 3. Freundlich isotherm plot for Pb<sup>2+</sup>

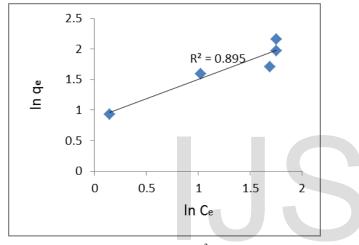


Fig. 4. Freundlich isotherm plot for  $Zn^{2+}$ 

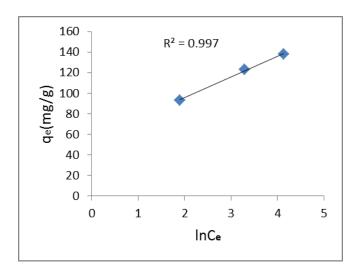


Fig. 5. Temkin isotherm plot for  $Pb^{2+}$ 

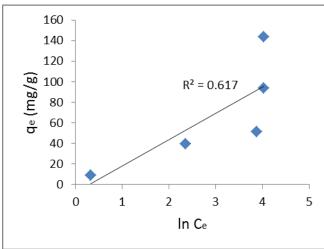


Fig. 6. Temkin isotherm plot for  $Zn^{2+}$ 

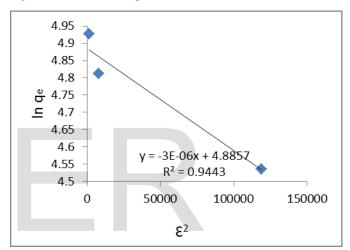


Fig.7. Dubinin-Radushkevich isotherm plot for Pb<sup>2+</sup>

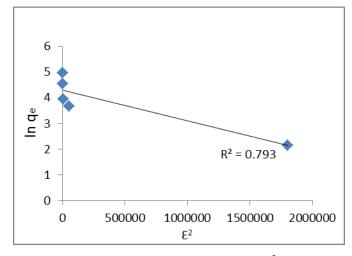


Fig. 8. Dubinin-Radushkevich isotherm plot for Zn<sup>2+</sup>

 $\label{eq:Table 1} Table \ 1$  Equilibrium sorption isotherm parameters for  $Pb^{2+}$  and  $Zn^{2+}$ 

Isotherm	Parameters	Pb <sup>2+</sup>	Zn <sup>2+</sup>
Langmuir	q <sub>m</sub>	142.857	100
	K <sub>L</sub>	0.777	0.068
	R <sub>L</sub>	0.068	0.006
	$\mathbb{R}^2$	0.995	0.99
Freundlich	K <sub>F</sub>	6.209	2.633
	1/n	0.178	0.631
	n	5.618	1.585
	$\mathbb{R}^2$	0.991	0.895
Temkin	b <sub>T</sub>	122.652	97.16
	A <sub>T</sub>	15.45	0.748
	$\mathbb{R}^2$	0.997	0.617
Dubinin-	K <sub>ad</sub>	3.00E-06	1.00E-06
Radushkevich	qs	132.29	73.626
	Е	707.109	408.248
	R <sup>2</sup>	0.944	0.793

#### 4.0 CONCLUSION

All applied isotherms fitted the adsorption data well for both Pb<sup>2+</sup> and  $Zn^{2+}$ . From the results obtained, it can be concluded that rice husk modified with phosphoric acid has a good potential as adsorbent for the removal of  $Pb^{2+}$  and  $Zn^{2+}$  from wastewater water. It was observed that the order of adsorption affinity on rice husk is  $Pb^{2+} >$  $Zn^{2+}$ . This is related to the difference in their electronegativity. Adsorption of rice husk surface is due to ion exchange at the surface level, as such, it is expected that the more electronegative metal will show a higher adsorption tendency. The electronegativity of Pb<sup>2+</sup> and  $Zn^{2+}$  is 2.33 and 1.65 respectively [2]. The adsorption of heavy metal with a larger ionic radius is greater than those with smaller radius [2]. The ionic radius of  $Pb^{2+}$  and  $Zn^{2+}$  is 1.33 and 0.88 respectively. The suitability of both Langmuir and Freundlich isotherms in representing the adsorption data for the sorption of  $Pb^{2+}$  and  $Zn^{2+}$  is an indication that a monolayer of metal ions was formed on the rice husk surface.

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